

# Enhanced Heat Transfer for FLiBe Blanket System Using Swirl Flow Method

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## 1. *Introduction*

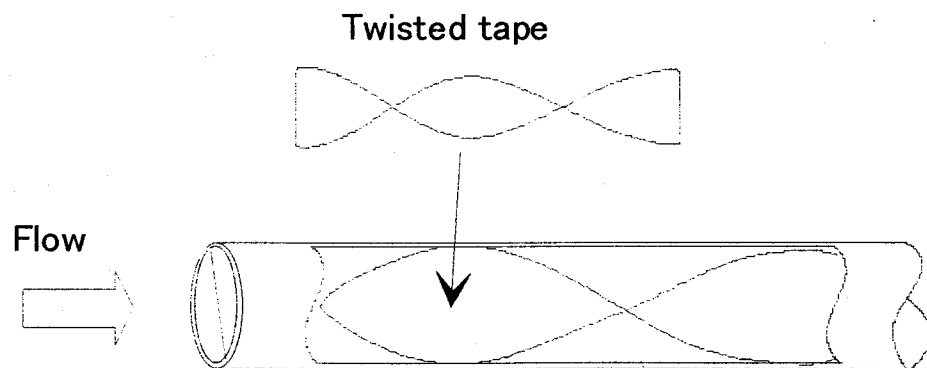
Development of high heat flux components



### Swirl tube

#### Factors of heat transfer enhancement

- ✧ Increase in mass flow rate
- ✧ Increase in wetted area
- ✧ Increase in relative velocity
- ✧ Heat transfer effect by secondary flow
  - ✧ Fin effect by the tape
  - ✧ Prevention of heat load concentration by swirling flow



## *2.Objective*

Heat transfer enhancement in swirl pipe flow is several times compared with smooth pipe.



Analogy estimation is insufficient for cooling performance.



It is difficult to predict cooling performance.

The reasons are as follows.

- ✧ Scale effect of experimental apparatus  
Method of temperature measurement
- ✧ Arrangement method of data
- ✧ Lack of numerical data

Main flow has swirling structure.



Secondary flow → Three dimensional flow

In previous numerical calculations, these complex secondary flows could not be reproduced.



Numerical simulation in laminar flow  
(not to use calculation assumptions)



Estimation of effects of the secondary flow  
on heat transfer enhancement.

- Qualitative estimation of secondary flow
- Quantitative estimation of cooling performance

### *3. Calculation method*

#### Assumptions

- ✧ Incompressible Newton steady flow
- ✧ Disregard for viscous dissipation
- ✧ Boussinesq approximation

#### Governing equations

Navier-Stokes equation  
Continuity equation  
Energy equation

Descartes coordinate

Tensor analysis

Twisted coordinate

## Finite difference method

Control volume method, Power-law scheme,  
SIMPLE, Forward difference

## Parameters

$Re, Pr, Nu, Gr, \gamma, X$
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Re : Reynolds number

Pr : Prandtl number

Nu : Nusselt number

Gr : Grashof number

$\gamma$  : Twist ratio

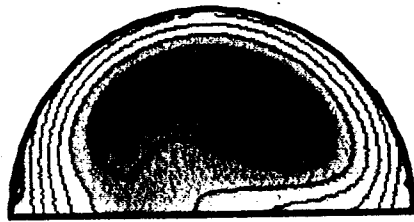
X : Dimensionless distance  
for axial direction

$\gamma \rightarrow \text{small}$   $\Rightarrow$  Highly Twist

#### 4. Calculation results and consideration

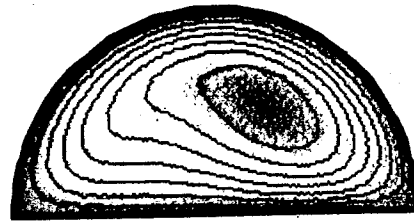
Qualitative estimations of flow field

$Re = 2000$ ,  $Pr = 3$ ,  $Gr = 0$ ,  $\gamma = 30$ ,  $X = 40$



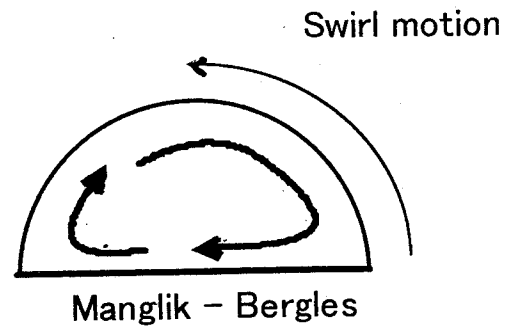
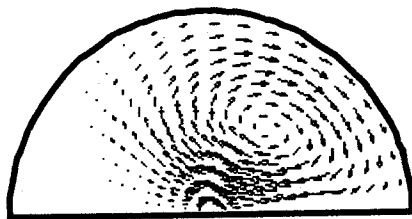
0.0 5.4

(a) Isothermal map



0.0 2.0

(b) Axial velocity map



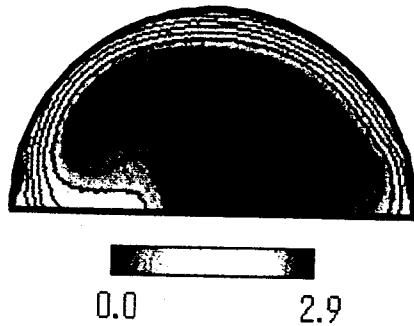
(c) Secondary flow

left: Present result

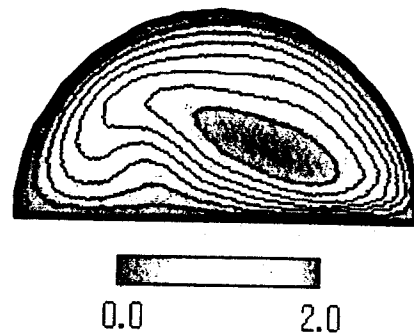
right: By experimental one ( $\gamma_0 \gg 1$ )

Fig.1: Flow pattern of low swirl effect

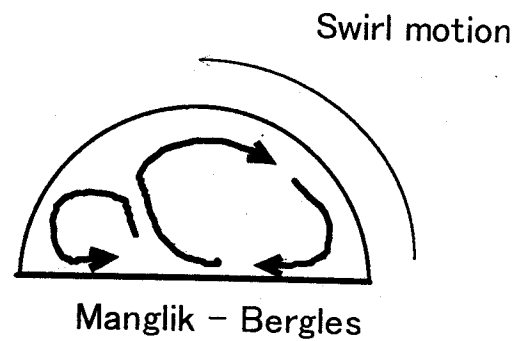
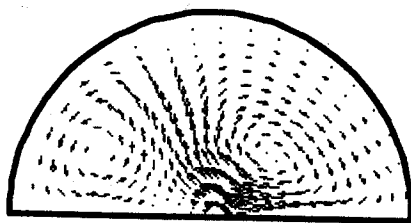
$Re = 2000, Pr=3, Gr=0, \gamma = 10, X=20$



(a) Isothermal map



(b) Axial velocity map



(c) Secondary flow

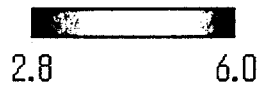
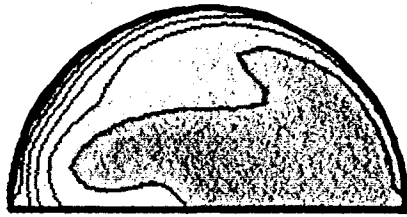
left: Present result

right: By experimental one ( $\gamma < \gamma_0$ )

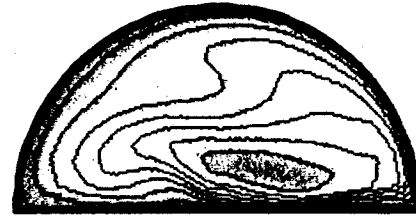
Fig.2: Flow pattern of middle swirl effect



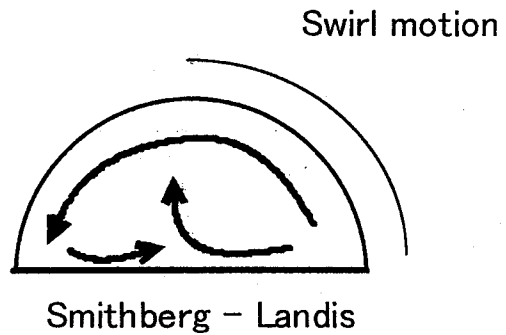
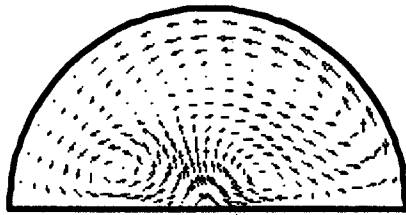
$$Re = 2500, Pr=3, Gr=0, \gamma = 5, X=5$$



(a) Isothermal map



(b) Axial velocity map



(c) Secondary flow

left: Present result

right: By experimental one (  $Re=1.4 \times 10^4$ ,  
 $\gamma = 10.4$  )

Fig.3: Flow pattern of high swirl effect

## Quantitative estimation for cooling performance

Estimation of averaged Nusselt number  
in heated region

$$\text{Nu} = 1.058 \text{Re}^{0.27} \text{Pr}^{0.27} + 0.205 \gamma^{-1.52} \text{Re}^{0.83} \text{Pr}^{0.38} \\ + 6.05 \text{Gr} \text{Re}^{1.65} \text{Pr}^{0.58}$$

$$\text{Nu}_{\text{Hong}} = 5.172 \left( 1 + 5.484 \times 10^{-3} \text{Pr}^{0.7} \text{Re}^{1.25} \gamma^{-1.25} \right)^{0.5}$$

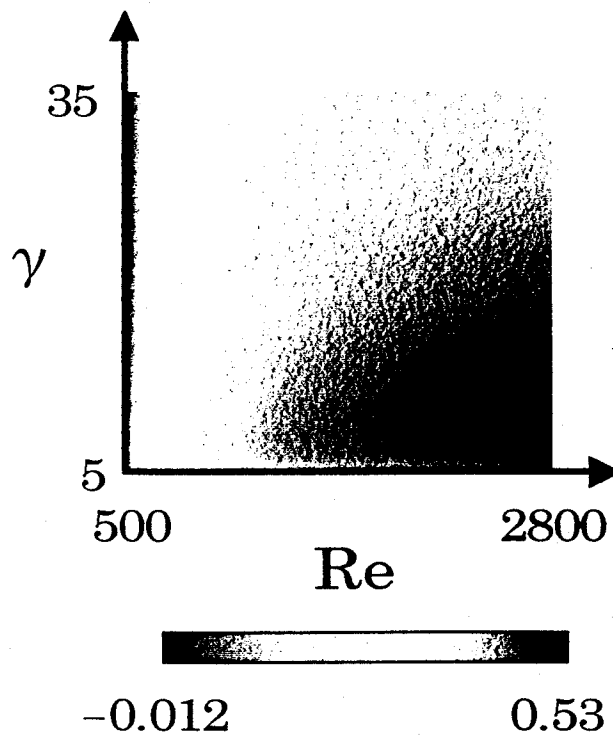


Fig.4: Deviation from Hong's result  
( $\text{Pr}=3$ ,  $\text{Gr}=2 \times 10^4$ )

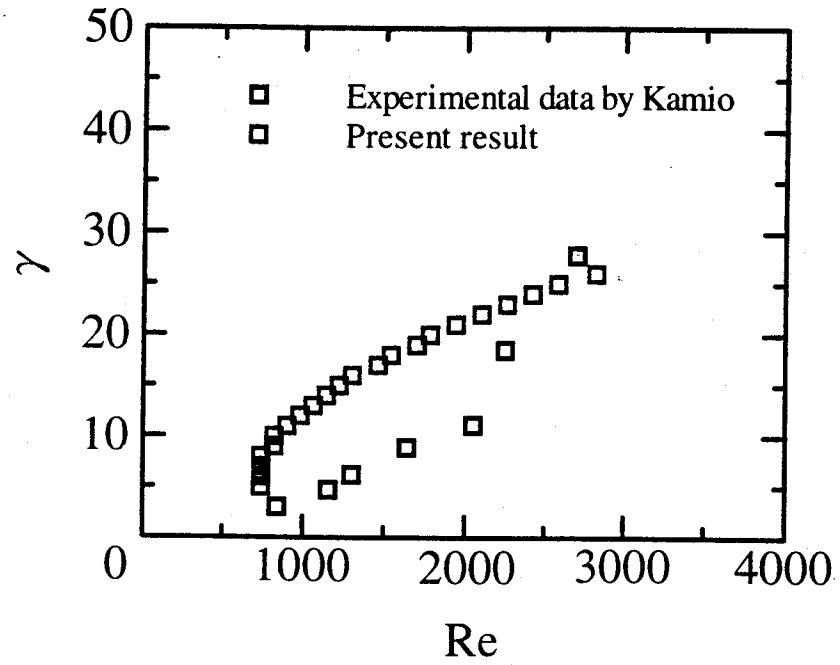
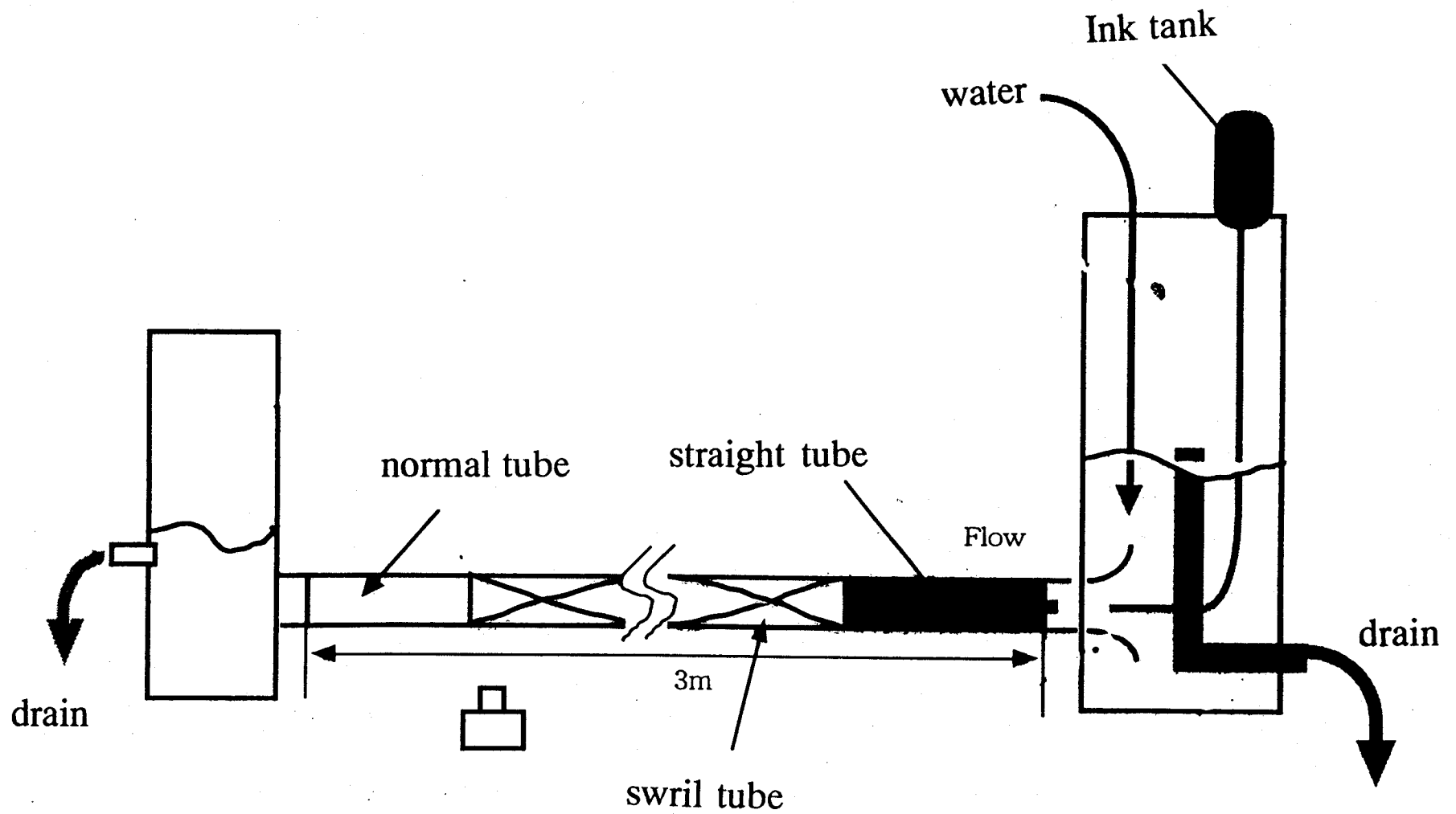
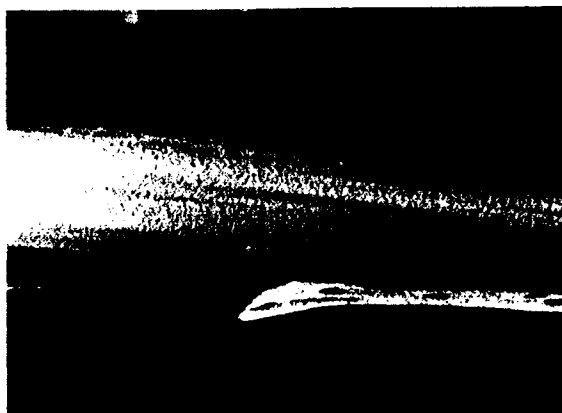


Fig.5: Distribution of critical  $Re$  number  
(  $Pr=3$ ,  $Gr=2 \times 10^4$  )



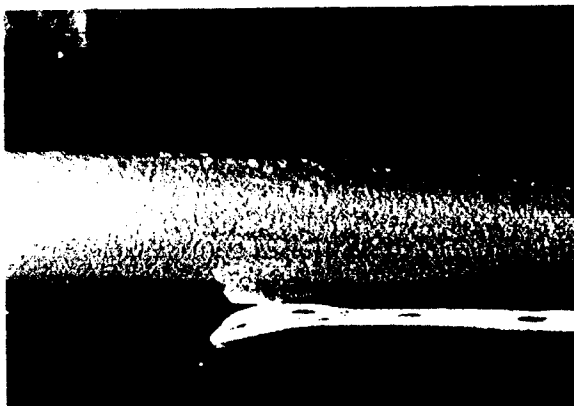
Experimental system



(a)  $Re_{Sw}=1638$

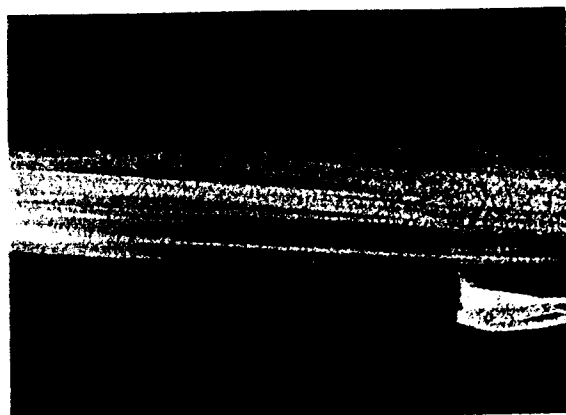


(b)  $Re_{Sw}=1693$

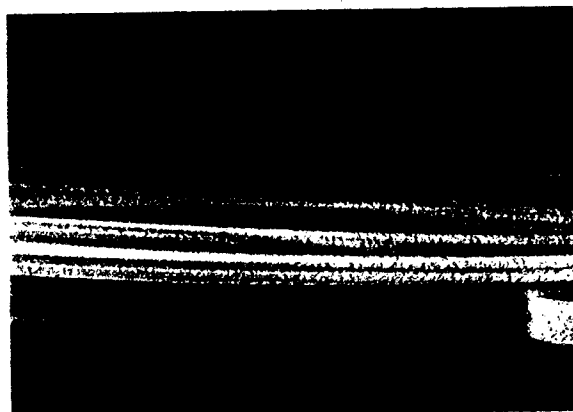


(c)  $Re_{Sw}=1771$

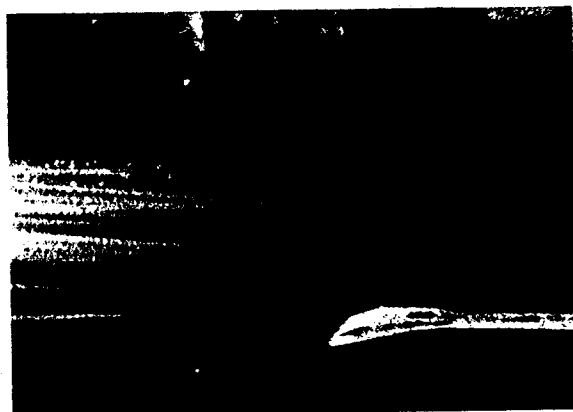
Figure  $\gamma=8.9$



(a)  $Re_{Sw}=1188$

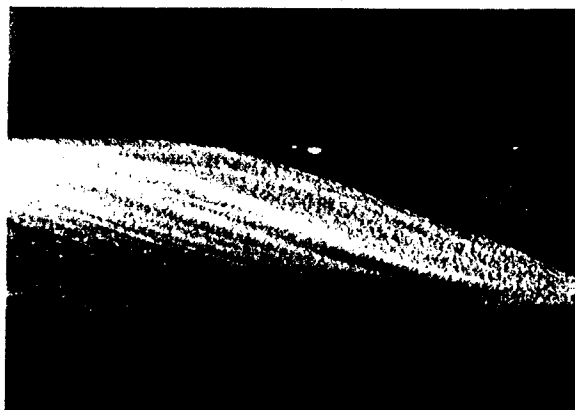


(b)  $Re_{Sw}=1344$

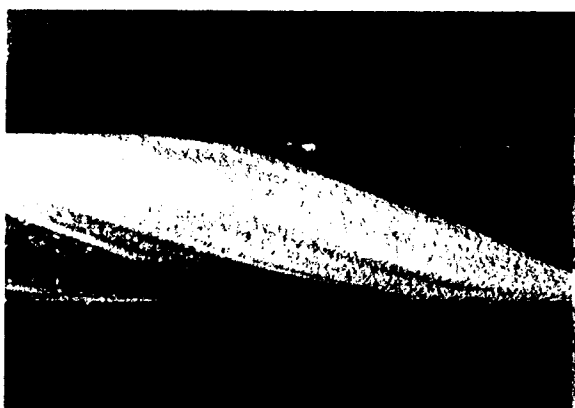


(c)  $Re_{Sw}=1550$

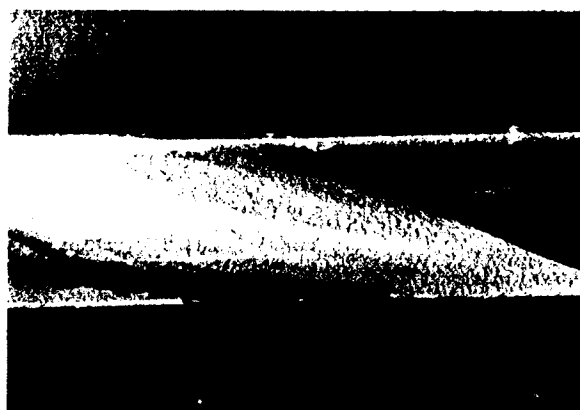
Figure  $\gamma=8.9$



(a)  $Re_{Sw}=600$

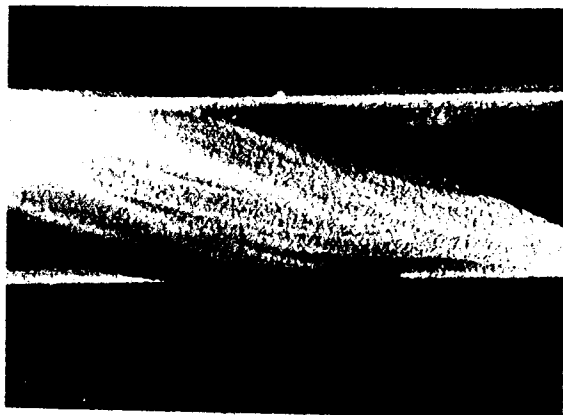


(b)  $Re_{Sw}=713$

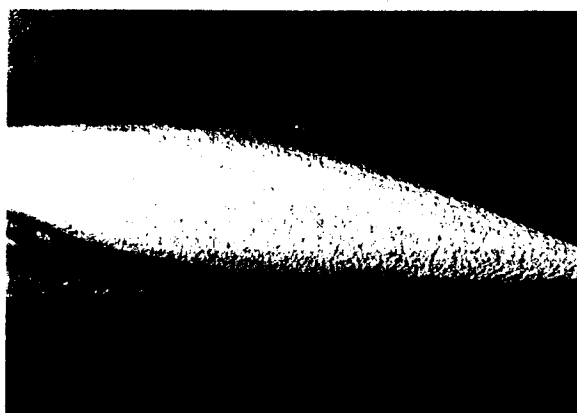


(c)  $Re_{Sw}=738$

Figure  $\gamma=3$



(a)  $Re_{Sw}=837$



(b)  $Re_{Sw}=872$



(c)  $Re_{Sw}=1168$

Figure  $\gamma=3$



# 作動流体 FLiBe

(  $Re=1500$   $Pr=35.6$   $y=5$  )

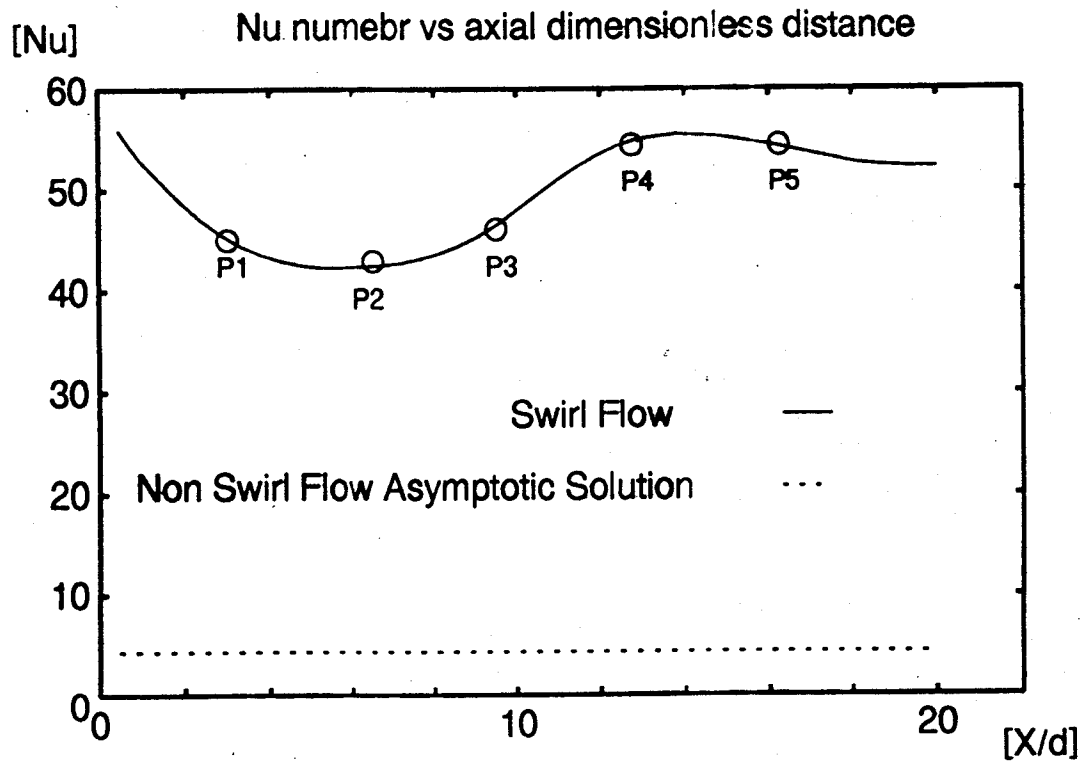


図 1: FLiBe における管軸方向 Nu 遷移

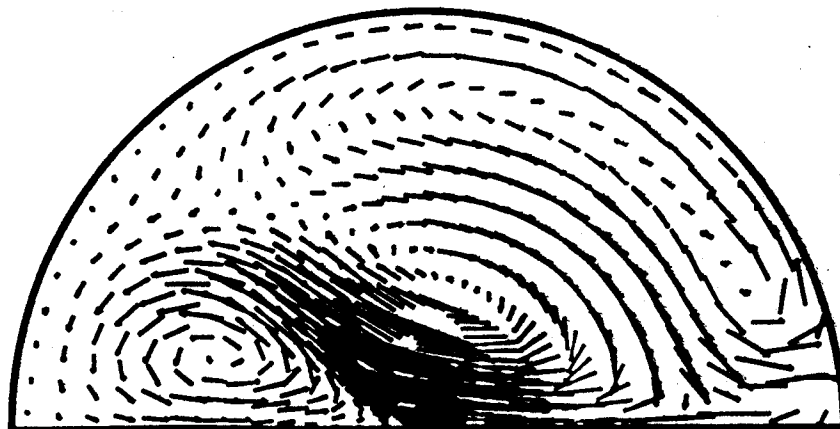


図 2: 断面速度分布 P1

# SWIRL DESIGN PROGRESS

## DESIGN HIGHLIGHTS OF SWIRL CONCEPT FOR ST CONFINEMENT CONFIGURATION

### ST Confinement Configuration Design and Preliminary Swirl Concept Operating Parameters.

ST (I) : Base Design

ST(II) : 50 % Lower Inboard  
Vertical Velocity

ST(III) : Base Design with 10 MW/m<sup>2</sup>  
Neutron Wall Loading.

\*Required pumping power for swirl  
concept in ST confinement  
configuration for a outboard liquid  
wall thickness of .3 m is < 30 MW.

\* Operating fluid may be recycled  
5 times for a average higher outlet  
temperature (~50 C higher) if there is  
a factor of two increase in the surface  
heat transfer coefficient.

	ST (I)	ST (II)	ST (III)
Major Toroidal Radius (m)	2.896	2.896	2.896
Minor Radius (m)	1.81	1.81	1.81
Plasma Aspect Ratio	1.6	1.6	1.6
Plasma Vertical Elongation	3.69	3.69	3.69
Outboard Fluid Azimuthal Inlet Velocity (m/s)	11.0	11.0	11.0
Outboard Fluid Vertical Inlet Velocity (m/s)	4.5	4.5	4.5
Outboard Average Coolant Velocity (m/s)	10.0	10.0	10.0
Outboard Maximum Flow Area (m <sup>2</sup> )	9.89	9.89	9.89
Av. Outboard Liquid Wall Thickness (m)	.3	.3	.3
Outboard Volumetric Flow Rate (m <sup>3</sup> /s)	98.9	98.9	98.9
Outboard Mass Flow Rate (kg/s)	1.94 10 <sup>5</sup>	1.94 10 <sup>5</sup>	1.94 10 <sup>5</sup>
Inboard Fluid Vertical Inlet Velocity (m/s)	15.0	10.0	10.0
Inboard Maximum Flow Area (m <sup>2</sup> )	4.4	4.41	4.41
Av. Inboard Liquid Wall Thickness (m)	.5	.5	.5
Inboard Volumetric Flow Rate (m <sup>3</sup> /s)	66.1	44.1	44.1
Inboard Mass Flow Rate (kg/s)	1.29 10 <sup>5</sup>	8.65 10 <sup>4</sup>	8.65 10 <sup>4</sup>
Fusion Power (MW)	3845.0	3845.0	4372.
Average Wall Load (MW/m <sup>2</sup> )	8.8	8.8	10.
Total Pumping Power (MW)	27.3	17.14	17.14
Average Temperature Rise (K)	5.17	8.61	9.38